## Hybrid 3D simulations on cylinder at Re=1M

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## Brief description

RANS closure term

$$\tau^{RANS} = \left(\overbrace{0}^{\rho}, \overbrace{0}^{\rho \mathbf{u}}, \overbrace{0}^{\rho E}, \overbrace{\tau: \nabla \mathbf{u} - \rho \epsilon}^{\rho k}, \overbrace{(C_1 \tau: \nabla \mathbf{u} - C_2 \rho \epsilon + E) T^{-1}}^{\rho \epsilon}\right)$$

**DDES** closure term  $\rho\epsilon$  is remplaced by  $\rho \frac{k^{3/2}}{l_{ddes}}$  where :

$$\mathfrak{l}_{ddes} = \frac{k^{\frac{3}{2}}}{\epsilon} - f_{ddes} \max\left(0, \frac{k^{\frac{3}{2}}}{\epsilon} - 0.65\Delta_{T}\right), \quad \begin{array}{l} f_{ddes} = 1 - \tanh((8r_{d})^{3}), \\ r_{d} = \frac{1 - \tanh((8r_{d})^{3})}{\epsilon^{2}y^{2}\max(\sqrt{\nabla u}:\nabla u, 10^{-10})} \end{array}$$

**VMS** closure term with dynamics coefficients  $C_s = C_s(\mathbf{x}, t)$  and  $Pr_t = Pr_t(\mathbf{x}, t)$ 

$$au^{DVMS}(W_{h}) = \left(0, \mathbf{M}_{S}(W_{h}, \phi_{h}^{'}), M_{H}(W_{h}, \phi_{h}^{'}), 0, 0\right)$$

where :

$$\begin{split} \mathbf{M}_{S}(W_{h},\phi_{i}') &= \sum_{T\in\Omega_{h}}\int_{T}\rho_{h}(\mathcal{C}_{s}\Delta_{T})^{2}|S'|\mathcal{D}(S')\nabla\phi_{i}'d\mathbf{x}, \\ M_{H}(W_{h},\phi_{i}') &= \sum_{T\in\Omega_{h}}\int_{T}\rho_{h}\frac{C_{p}(\mathcal{C}_{s}\Delta_{T})^{2}}{P_{t}}|S'|\nabla T'\cdot\nabla\phi_{i}'d\mathbf{x} \end{split}$$

and  $\phi'_h = \phi_h - \overline{\phi_h}$  where  $\overline{\phi_h}$  is computed from macro cells. Hybrid description

$$\left(\frac{\partial \overline{W}_{h}}{\partial t}, \chi_{i}\right) + \left(\nabla \cdot F(\overline{W}_{h}), \chi_{i}\right) = \theta\left(\tau^{C}(\overline{W}_{h}), \phi_{i}\right) + (1 - \theta)\left(\tau^{DVMS}(W_{h}^{'}), \phi_{i}^{'}\right).$$
$$\tau^{C} \in \{\tau^{RANS}, \tau^{DDES}\}$$

## Hybridation function

#### Definition of blending function

$$\theta = 1 - f_{ddes}$$



Figure – Comparaison between  $\theta = 1 - f_{ddes}$  blending function, on left used for hybrid DDES and on right used for hybrid RANS.

Zonal approach with length scale

$$heta = \exp\left(-rac{1}{2\epsilon_0}d(\mathbf{x},V_{k,\epsilon})^2
ight),$$

where  $V_{k,\epsilon} = \{ x \in \Omega_f \mid \frac{k^{3/2}(x)}{\epsilon(x)} < \Delta_{les} \}$ 



Figure - Blending surface.

Blending function with protection zone

$$\theta = 1 - f_{ddes} \times (1 - \overline{\theta}),$$



Figure - Hybrid RANS blending surface.

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## Simulation with the wall law at Reynolds 1M

Reichardt wall law :

$$U^{+} = \frac{1}{\kappa} \ln \left(1 + \kappa y^{+}\right) + 7.8 \left[1 - \exp \left(\frac{-y^{+}}{11}\right) - \frac{-y^{+}}{11} \exp \left(\frac{-y^{+}}{3}\right)\right]$$

Simulation set up :

- mach number : 0.1 (subsonic flow)
- reference pressure : 101300  $\rm [N/m^2]$
- density : 1.22  $[kg/m^3]$



Figure – Computationnal domain on left, size of cell *h* close to the cylinder on the rigth computed such that :  $h\frac{Re}{20} = y^+ = 20 \Rightarrow h = 4.10^{-4}$ .

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Name	Mesh size	<i>y</i> <sup>+</sup>	⊂ <sub>d</sub>	$c'_l$	$-\overline{c}_{pb}$	<u>L</u> r	$\overline{\theta}$
Present simulation							
DDES $k - \epsilon$ Goldberg	4.8M	100	0.20	0.03	0.22	0.87	138
DDES/ DVMS Smagorinsky							
$f = 1 - \tanh((8r_d)^3)$ et $\overline{\theta} = \tanh(\left(\frac{\Delta_T}{k^{3/2}}\epsilon\right)^2)$	4.8M	100	0.20	0.016	0.22	0.82	135
$f = 1 - \tanh((8r_d)^{3}) \text{ et } \overline{\theta} = \tanh(\left(\frac{\Delta_T}{k^{3/2}}\epsilon\right)^{2})$	4.8M	200	0.13	0.015	0.05	0.82	135
$\theta = \exp(-\frac{1}{2\epsilon}d(r, V)^2)$	4.8M	100	0.20	0.005	0.24	0.92	132
$\theta = \exp(-\frac{1}{2\epsilon}d(r, V)^2)$	4.8M	200	0.14	0.001	0.05	0.58	144
$\theta = 1 - \tanh((8r_d)^{3})$	4.8M	100	0.20	0.01	0.21	0.82	133
$\theta = 1 - \tanh((8r_d)^{3})$	4.8M	200	0.14	0.01	0.04	0.58	142
Other simulations							
Catalano [1]	2.3M	-	0.31-0.40	-	0.32-0.41		
LES Kim [3]	6.8M	-	0.27	0.12	0.28	-	108
Expériences							
Gölling [9]						-	130
Zdravkovich [8]			0.2-0.4	0.1-0.15	0.2-0.34		

Table – Bulk coefficient of the flow around a circular cylinder at Reynolds number 1M,  $\overline{\underline{C}}_d$  holds for the mean drag coefficient,  $C'_l$  is the root mean square of lift time fluctuation,  $\overline{C}_{p_b}$  is the pressure coefficient at cylinder basis,  $\overline{L_r}$  is the mean recirculation lenght,  $\overline{\theta}$  is the mean separation angle.

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Name	Mesh size	<i>y</i> <sup>+</sup>	$\overline{C}_d$	$c'_l$	$-\overline{C}_{pb}$	$\overline{L_r}$	$\overline{\theta}$
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DDES/ DVMS Smagorinsky							
$f = 1 - \tanh((8r_d)^{3}) \text{ et } \overline{\theta} = \tanh(\left(\frac{\Delta T}{k^{3/2}}\epsilon\right)^{2})$	4.8M	100	0.20	0.016	0.22	0.82	135
$f = 1 - \tanh((8r_d)^{3}) \mathbf{et} \ \overline{\theta} = \tanh(\left(\frac{\Delta_T}{k^{3/2}}\epsilon\right)^2)$	4.8M	200	0.13	0.015	0.05	0.82	135
$\theta = \exp(-\frac{1}{2\epsilon}d(r, V)^2)$	4.8M	100	0.20	0.005	0.24	0.92	132
$\theta = \exp(-\frac{\mathbf{\hat{1}}}{2\epsilon}d(r, V)^{2})$	4.8M	200	0.14	0.001	0.05	0.58	144
$\theta = 1 - \tanh((8r_d)^{3})$	4.8M	100	0.20	0.01	0.21	0.82	133
$\theta = 1 - \tanh((8r_d)^{3})$	4.8M	200	0.14	0.01	0.04	0.58	142
RANS / DVMS Smagorinsky							
$f = 1 - \tanh((8r_d)^{3}) \text{ et } \overline{\theta} = \tanh(\left(\frac{\Delta_T}{k^{3/2}}\epsilon\right)^{2})$	4.8M	100	0.24	0.05	0.22	0.62	133
$f = 1 - \tanh((20r_d)^{3}) \text{ et } \overline{\theta} = \tanh((20r_d)^{3})$	4.8M	100	0.24	0.06	0.23	0.58	133
$f = 1 - \operatorname{tanh}((8r_d)^{3})$ et $\overline{\theta} = \operatorname{tanh}((8r_d)^{3})$	4.8M	100	0.24	0.06	0.21	0.60	134
$\theta = \exp(-\frac{1}{2\epsilon}d(r, V)^2)$	4.8M	100	0.20	0.02	0.17	0.78	134
$\theta = 1 - \tanh((8r_d)^{3})$	4.8M	100	0.25	0.06	0.19	0.72	133
Other simulations							
Catalano [1]	2.3M	-	0.31-0.40	-	0.32-0.41		
LES Kim [3]	6.8M	-	0.27	0.12	0.28	-	108
Expériences							
Gölling [9]						-	130
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Table – Bulk coefficient of the flow around a circular cylinder at Reynolds number 1M,  $\overline{\underline{C}}_d$  holds for the mean drag coefficient,  $C'_l$  is the root mean square of lift time fluctuation,  $\overline{C}_{p_b}$  is the pressure coefficient at cylinder basis,  $\overline{L_r}$  is the mean recirculation lenght,  $\overline{\theta}$  is the mean separation angle.

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Figure - Recirculation zone comparaison between hybrid models (WL case).

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Name	Mesh size	y <sup>+</sup>	$\overline{C}_d$	$c'_{l}$	$-\overline{C}_{pb}$	Lr	$\overline{\theta}$
Present simulation							
DDES $k - \epsilon$ Goldberg WL	4.8M	100	0.20	0.03	0.22	0.87	138
DDES $k - \epsilon$ Goldberg ITW	4.8M	100	0.50	0.06	0.54	1.22	103
DDES/ DVMS Smagorinsky WL	4.8M	100	0.20	0.016	0.22	0.82	135
DDES/ DVMS Smagorinsky ITW	4.8M	100	0.51	0.07	0.28	0.85	110
RANS / DVMS Smagorinsky WL	4.8M	100	0.24	0.05	0.22	0.62	133
RANS / DVMS Smagorinsky ITW	4.8M	100	0.47	0.08	0.34	0.62	110
Other simulations							
Catalano [1]	2.3M	-	0.31-0.40	-	0.32-0.41		
LES Kim [3]	6.8M	-	0.27	0.12	0.28	-	108
Expériences							
Gölling [9]						-	130
Zdravkovich [8]			0.2-0.4	0.1-0.15	0.2-0.34		

#### Result summary and comparaison with ITW

Table – Bulk coefficient of the flow around a circular cylinder at Reynolds number 1M,  $\overline{\underline{C}}_d$  holds for the mean drag coefficient,  $C'_l$  is the root mean square of lift time fluctuation,  $\overline{C}_{p_b}$  is the pressure coefficient at cylinder basis,  $\overline{L_r}$  is the mean recirculation lenght,  $\overline{\theta}$  is the mean separation angle.



Figure - Recirculation zone comparaison between hybrid models (ITW case ).

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#### Pressure coefficient



Figure – Distribution of mean pressure as a function of polar angle. Comparaison between experiment. Wall law on the left and integration to the wall on the right.

Velocity profile



Figure – On the top longitudonal velocity profile at x/D = 1, and on bottom the transverse velocity.

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Wall Law Q-criteria



Figure – Q-critera contour using velocity color scale.

Integration to the Wall Q-criteria



Figure – Q-critera contour using velocity color scale.

Conclusions and things to do

- Hybrid function with protection zone give better results,
- surface pressure coefficient is close to experimental data for WL,
- Bulks coefficients are good with RANS/DVMS model,
- Improve blend function to catch eddies at starting region of the wake,

• Test influence of WALE SGS model.

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